

Heimdal Brae De-Waxing Operation

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Heimdal Brae Wax Removal Summary

Removing large accumulations of wax using an aggressive high-friction pig with bypass



Presentation contents

- Part 1:
 - System & History



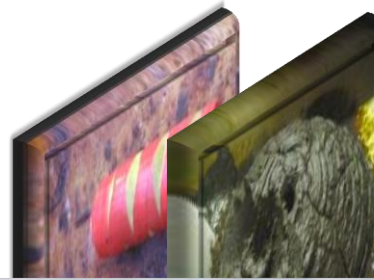
Presentation contents

- Part 1:
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 - Pipeline conditions



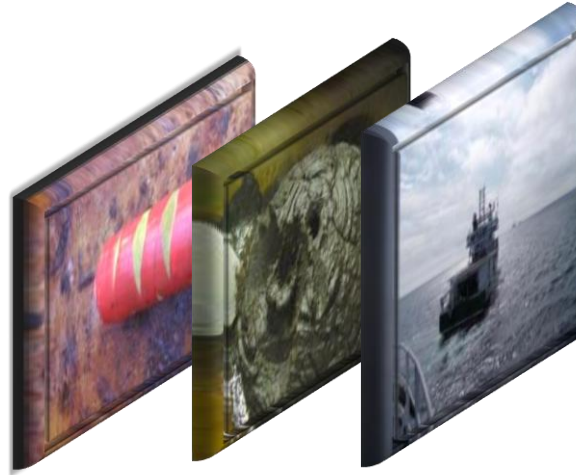
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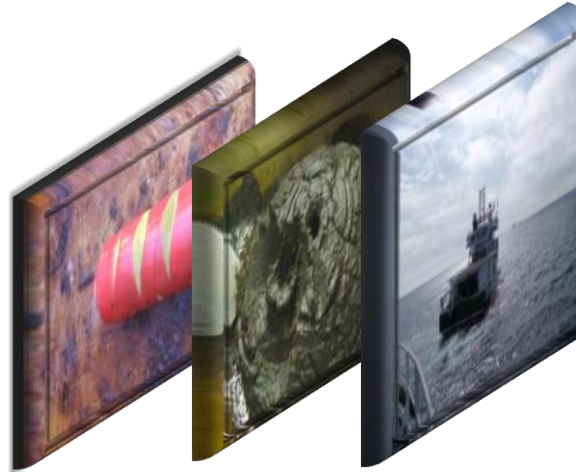
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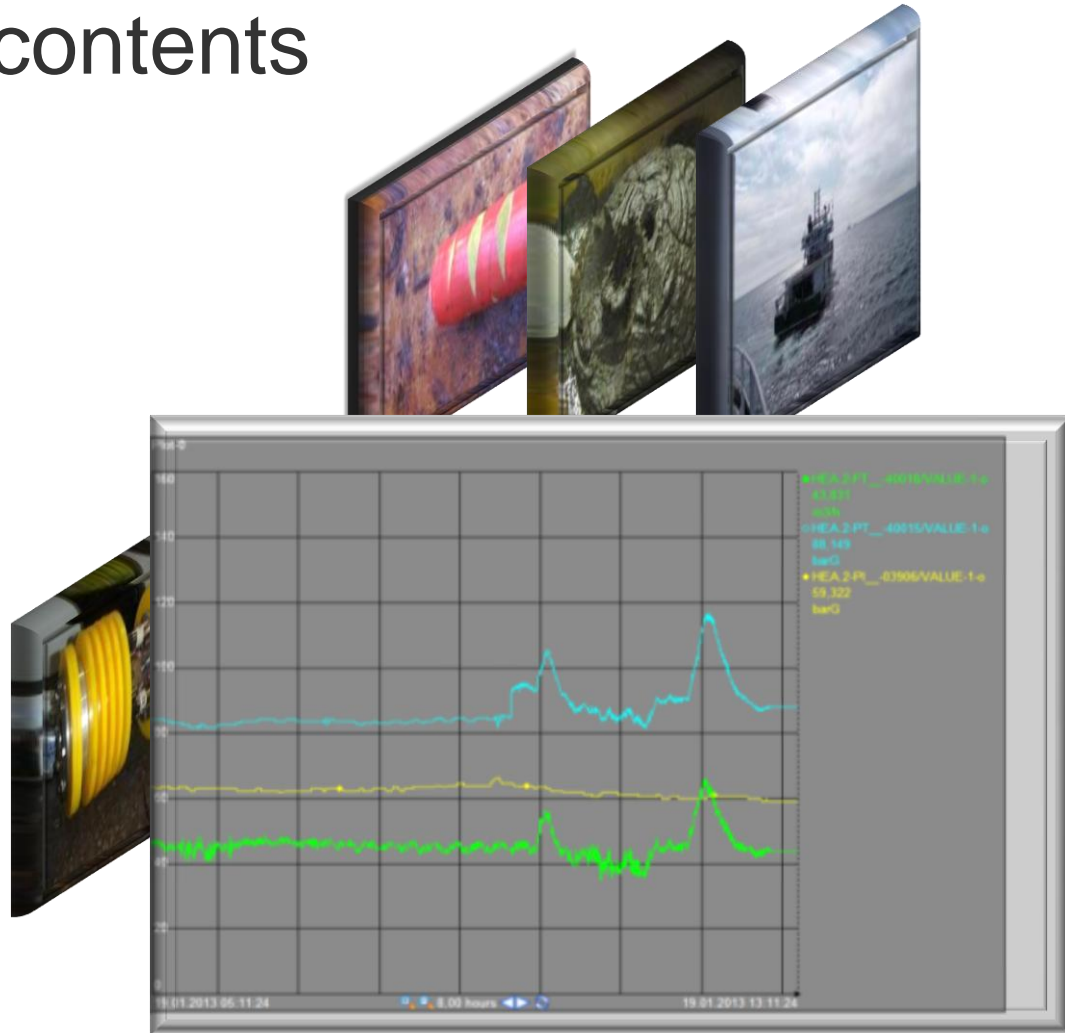
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- Part 2:
 - Pig design



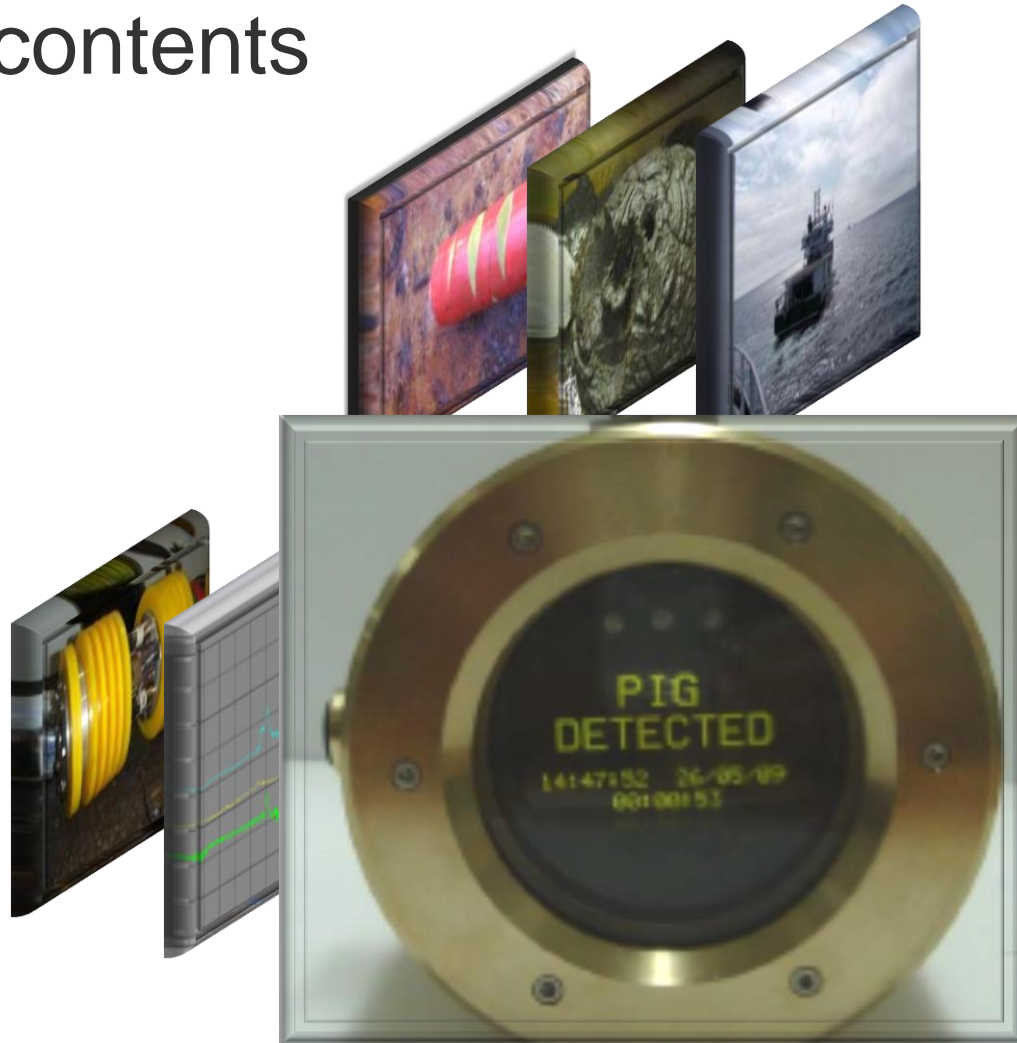
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 - Observations

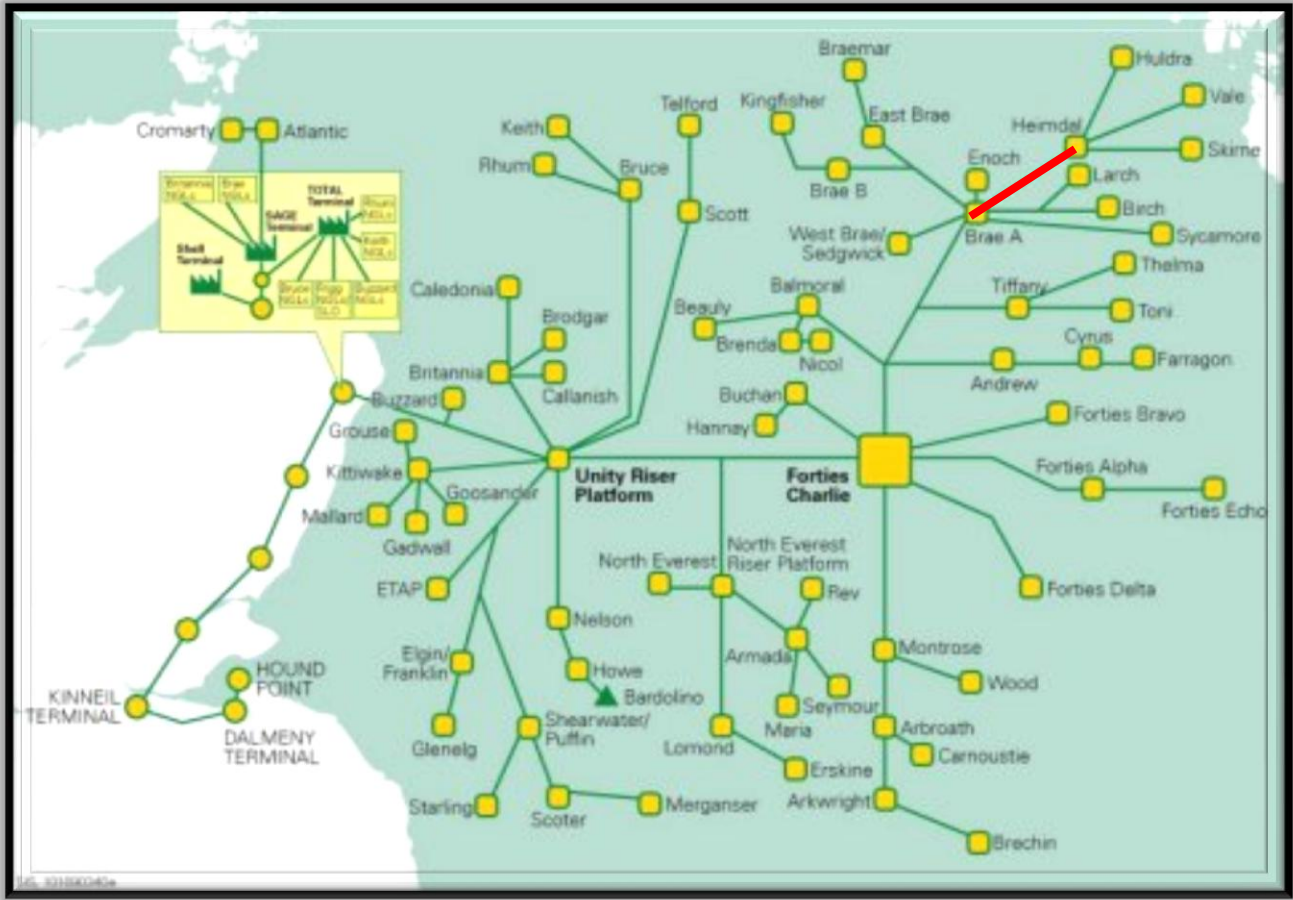


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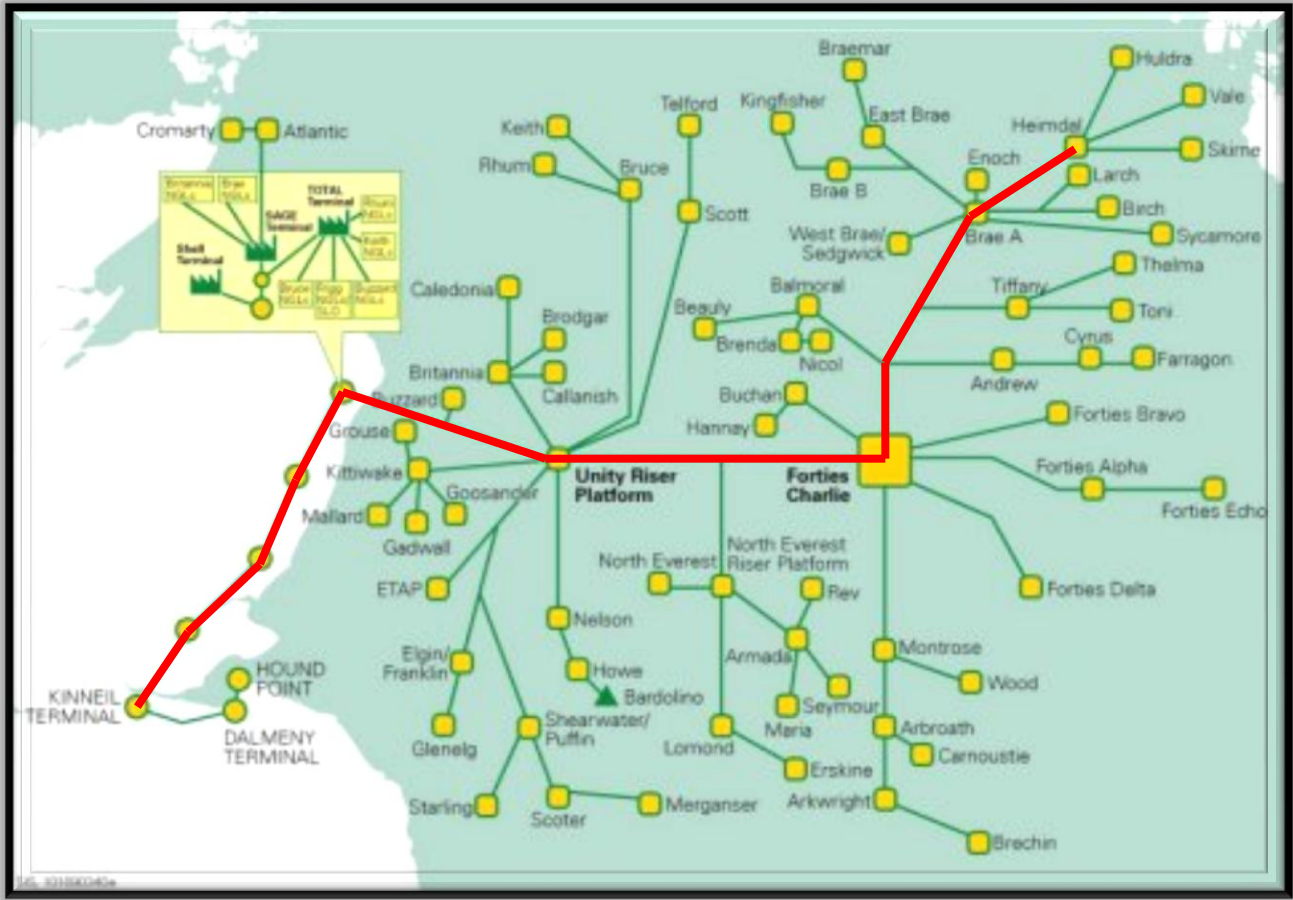
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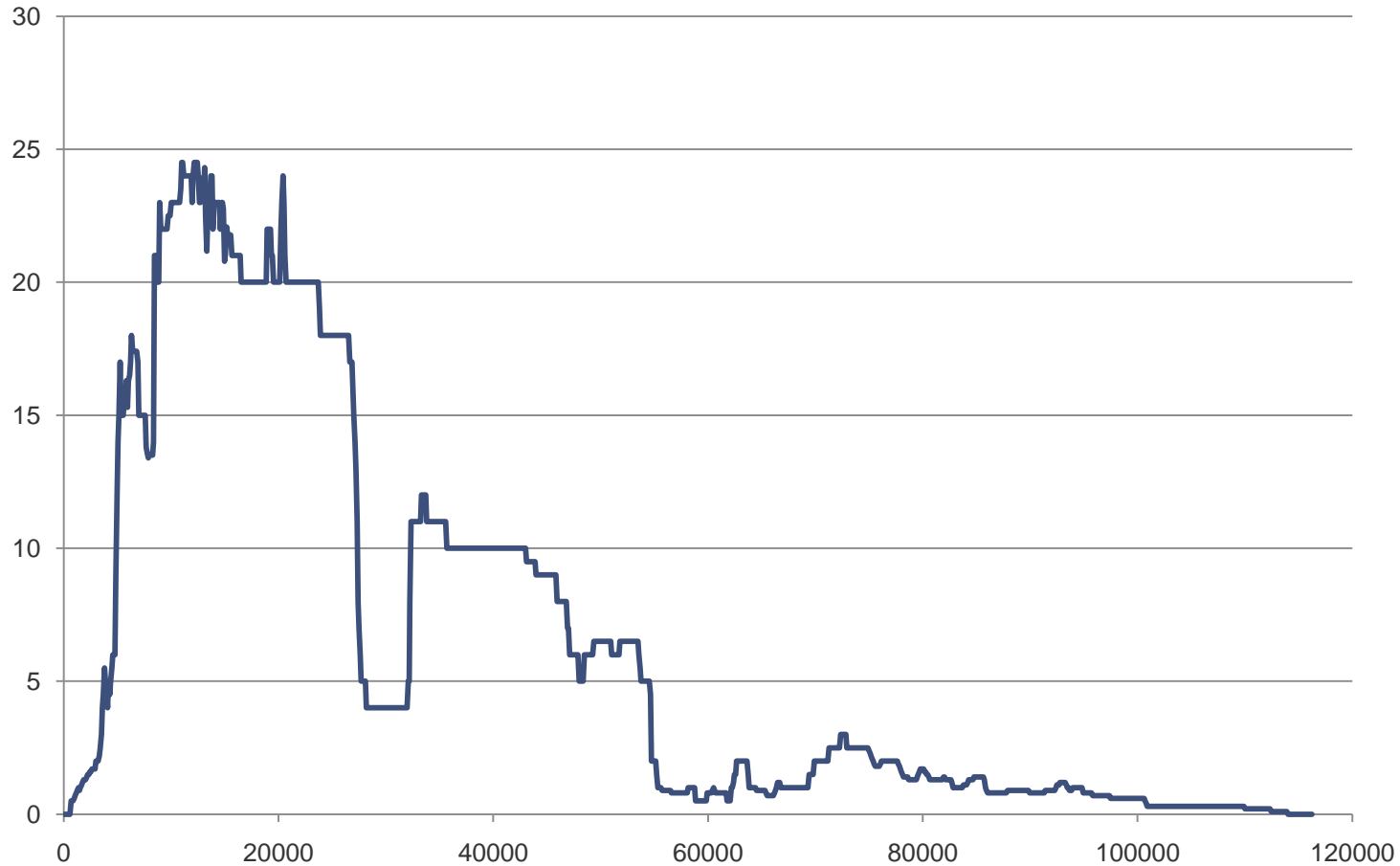
System



System



Total Wax Volume = 350 m³ (ca)



From Heimdal to Kinneil

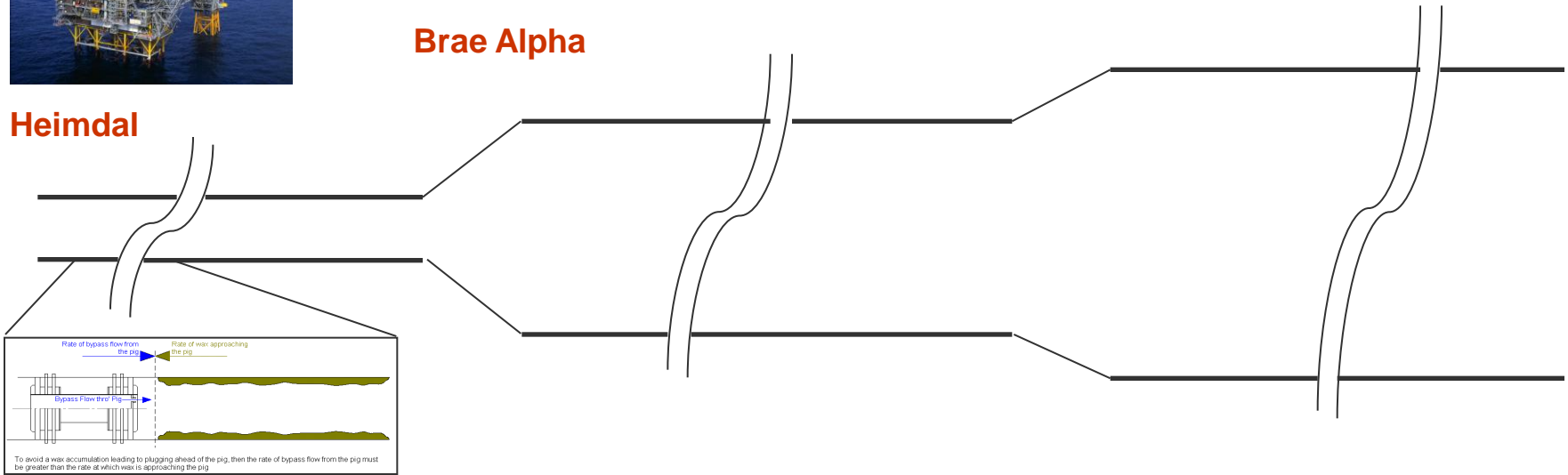


Heimdal

Brae Alpha

Forties Charlie

Kinneil



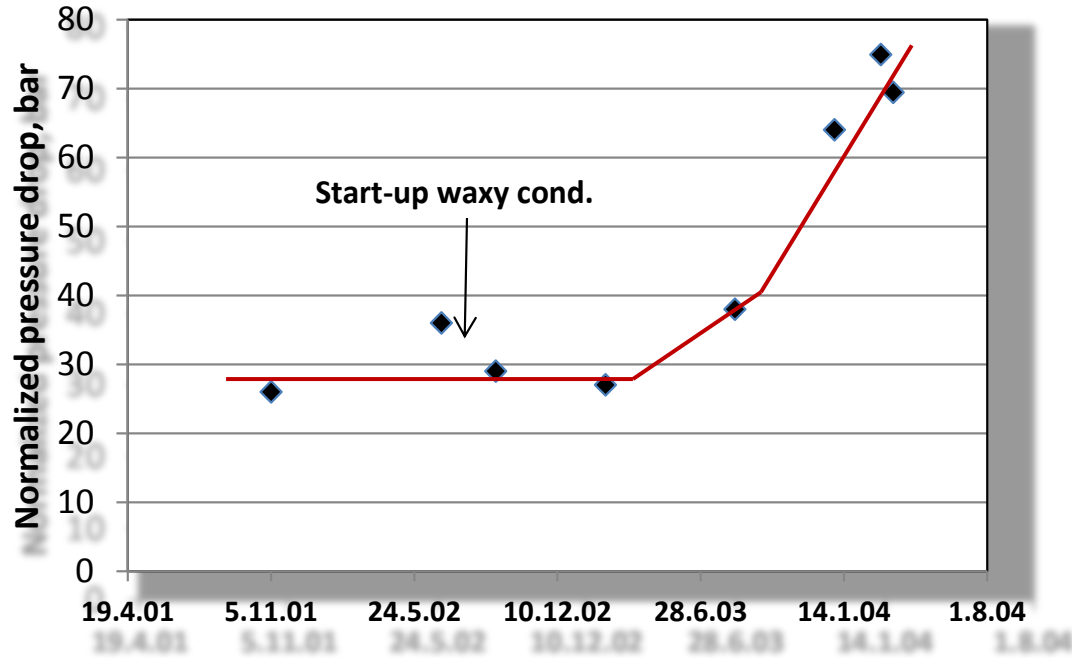
116 km
ID = 197 mm (8")
Turbulent

117 km
ID = 710 mm (28")
Laminar

169 km
ID = 860 mm (34")
Turbulent

Introduction of Vale fluids in 2002

Before 2002, no wax and no pigging performed. Then Vale field started up with high wax content.



- Build up of line differential pressure was insignificant until 2004

Pigging started early 2004 using foam pigs



First stuck foam pig April 2004

2004 - 2008

- Foam pigging program
- Stuck pigs



2008

- Fill and soak operation
- Chemical dissolvant
- Very good effect in laboratory
- Only minor effect in field



2008 - 2010

- Foam pigging
- Stuck pigs



2010: Aggressive pigging!

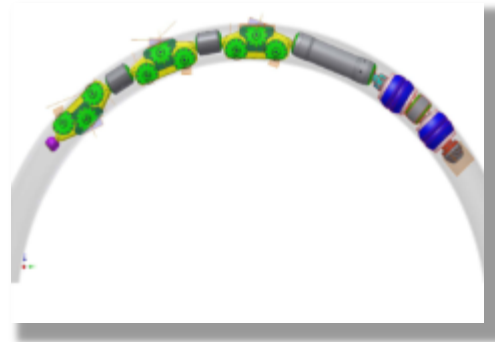
Why change strategy?

1. The pipeline NEEDS to become wax free due to inspection requirements
2. Progressive approach with foam pigs does not work

Two Alternatives for consideration:

1. Hydraulically Activated Power Pig (HAPP)
 - Limited experience
 - Assumed best for downstream facilities

2. High Friction Jetting Pig (HFJP)
 - Well proven technology
 - New application



Overall risk was evaluated together with our downstream partners, and the HAPP was chosen

HAPP pigging operation January 2012

Markland tests before and after

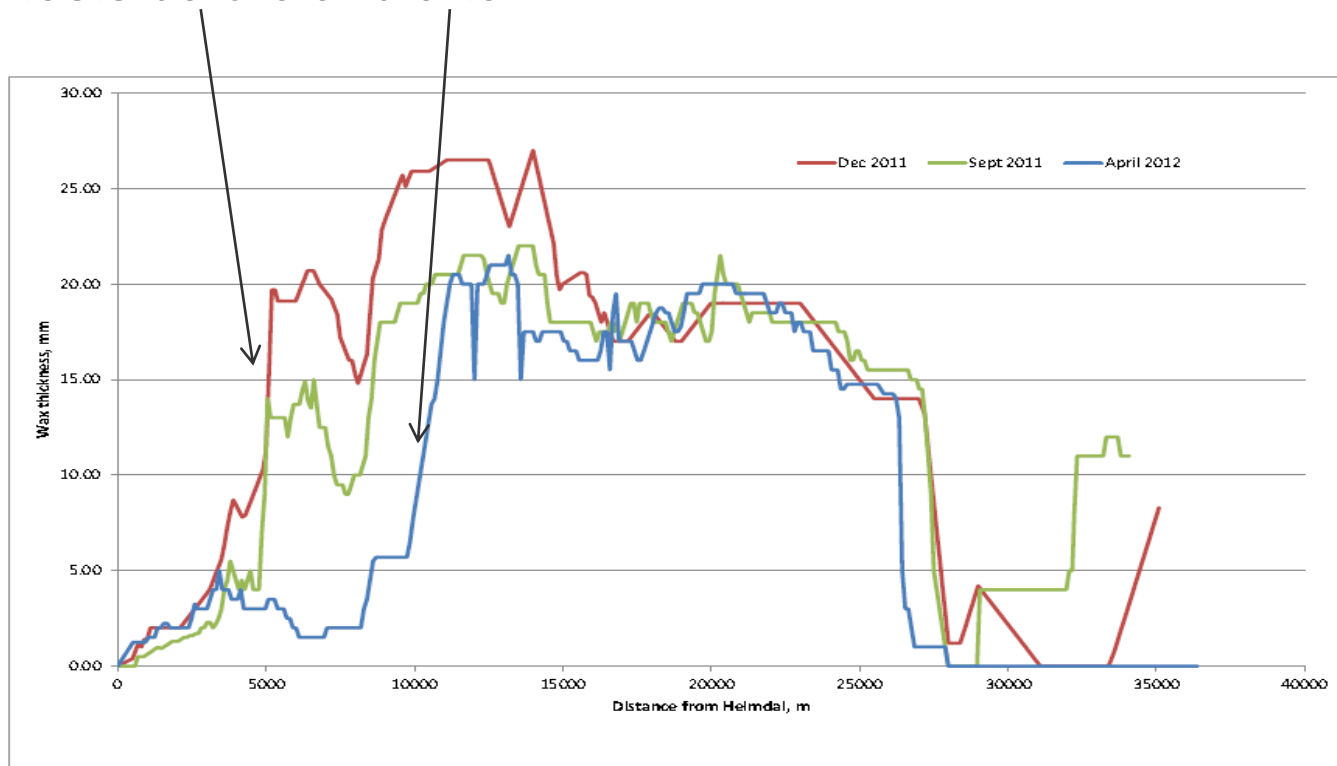
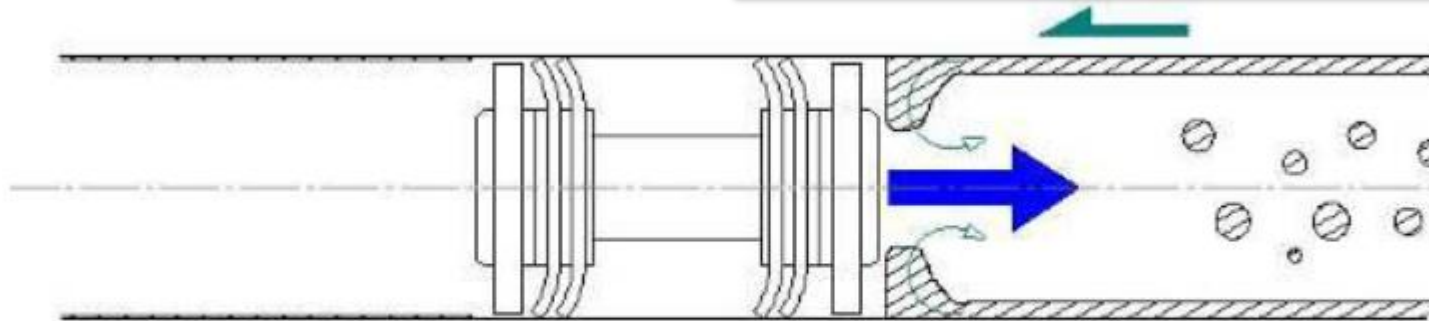


Figure 1. Wax thickness as function of distance from Heimdal, give as an evenly distributed layer around the pipe perimeter.

Pig stopped 15.01.12 at 8357 m

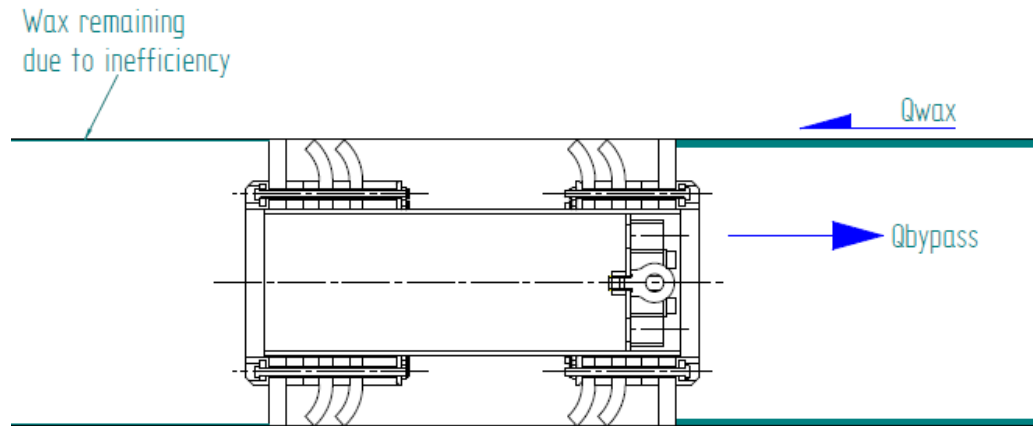
Estimated wax removed by HAPP = 80 m³
Remaining wax in pipeline = approx 350 m³

Decide to go for High Friction Jetting Pig



Wax piles up ahead of the pig and is blown forward by the central bypass

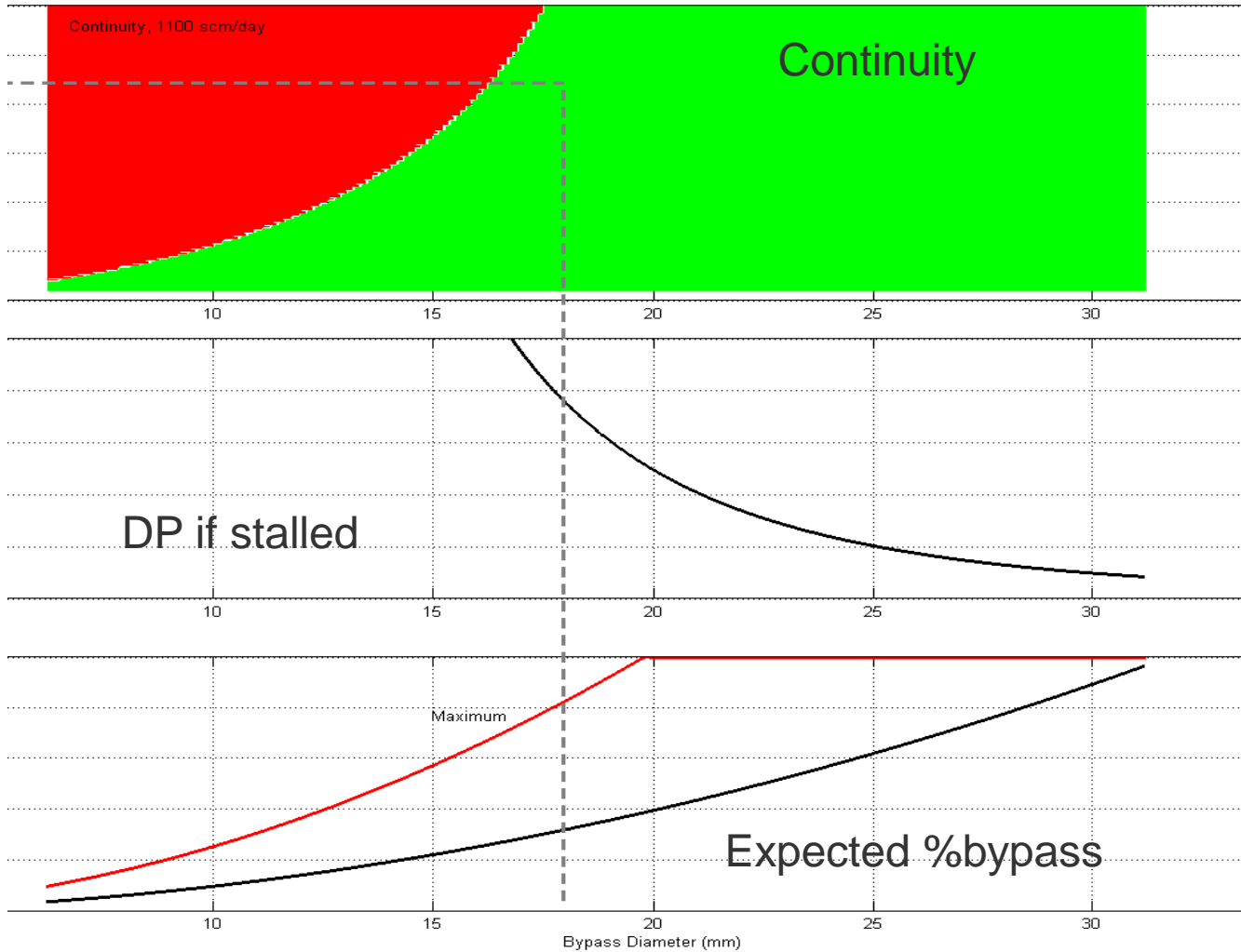
Basis of design



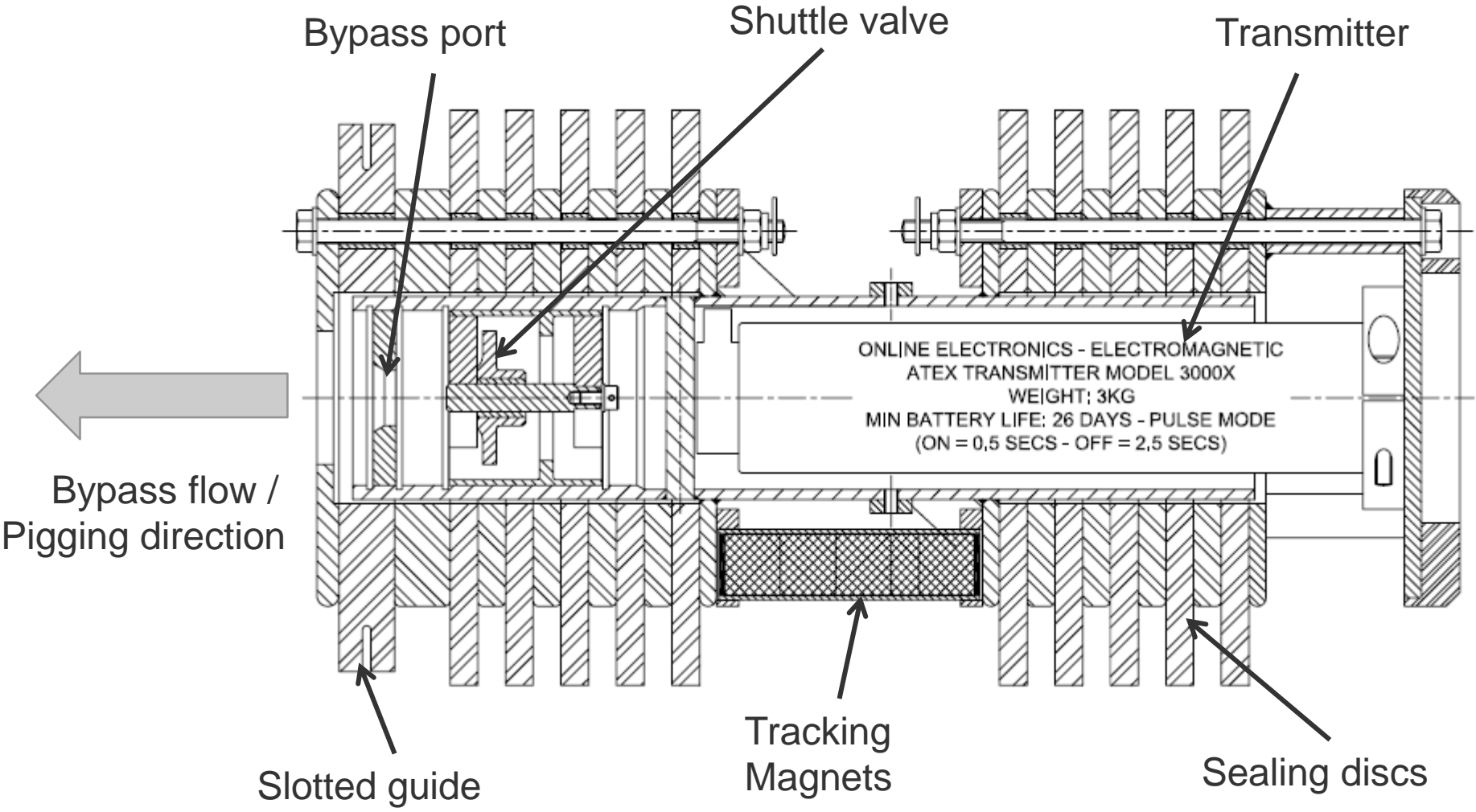
$$Q_{bypass} > Q_{wax} \quad \text{Green Circle}$$

$$Q_{wax} > Q_{bypass} \quad \text{Red Circle}$$

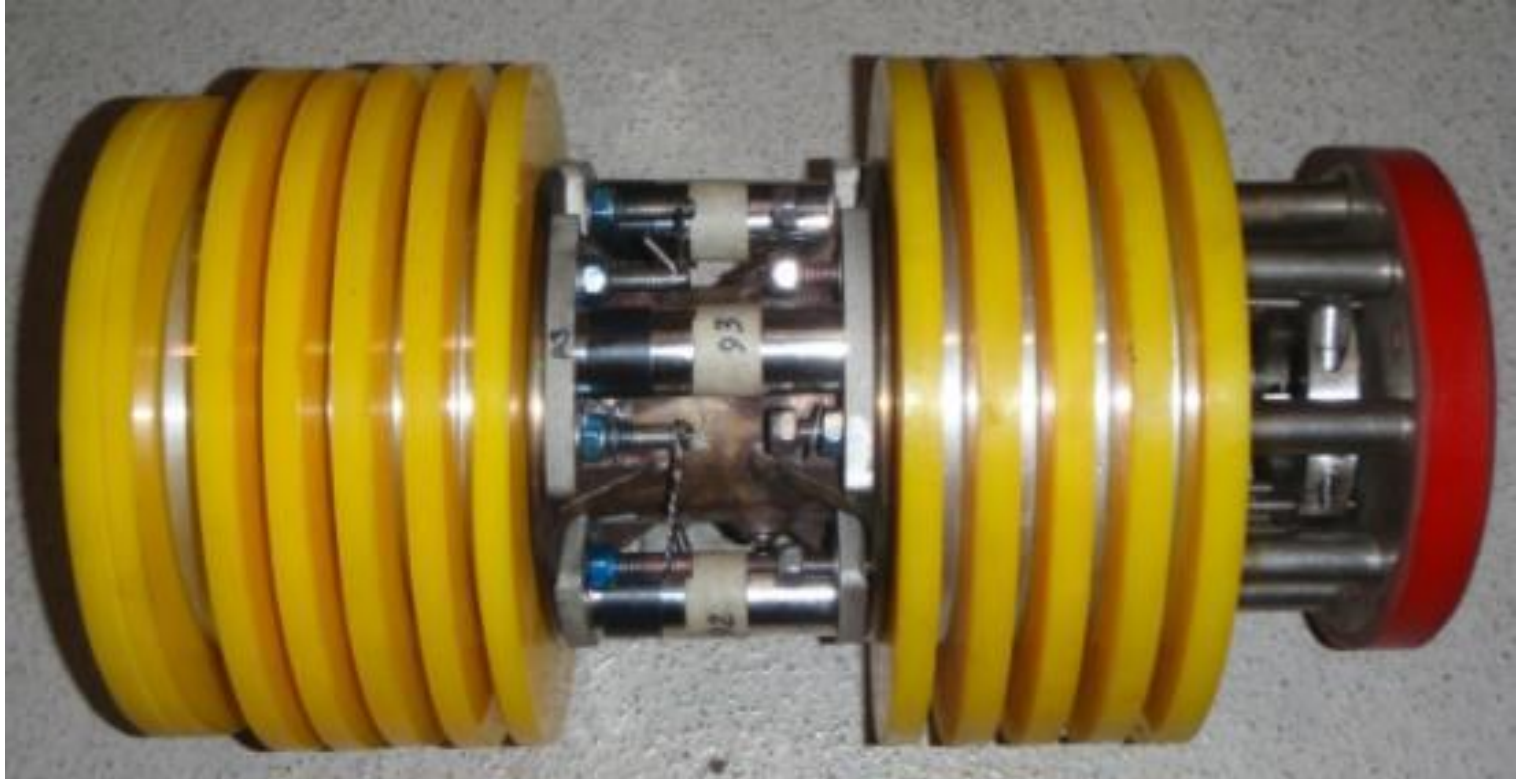
Continuity Principle (5 bar HF Pig, 18 mm port)



Pig Design



Final pig ready for deployment

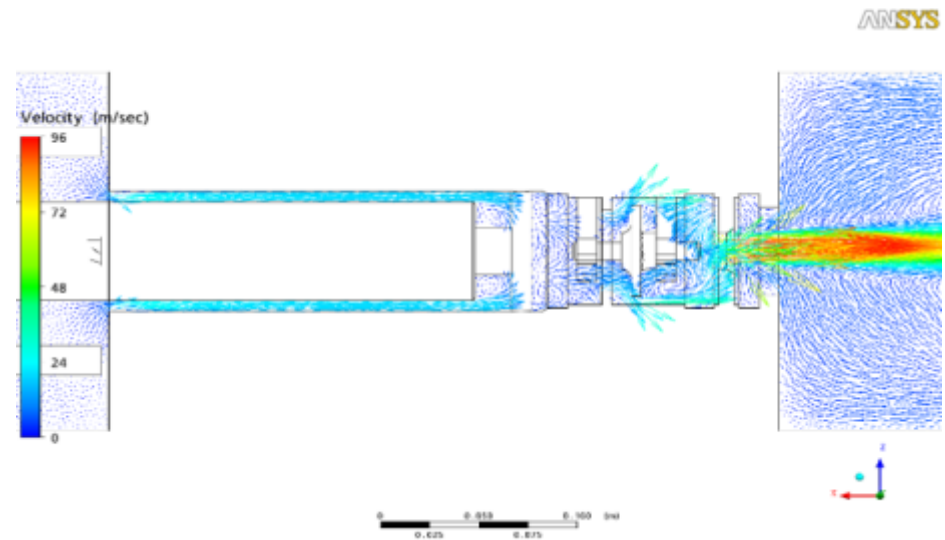


Testing and Validation

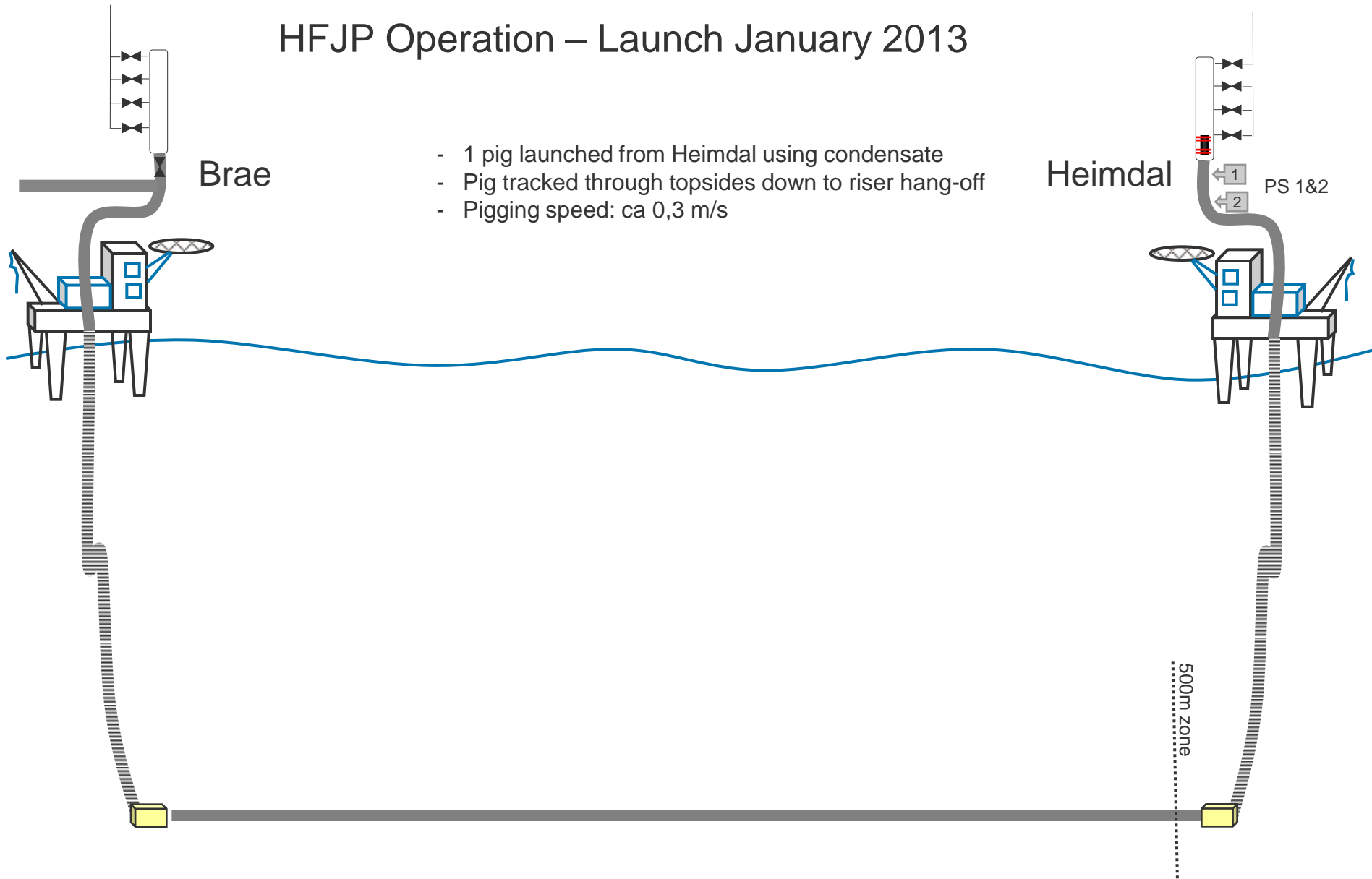


Other assurance

- Piggability studies (Negotiation of line components);
- Slurry study (transportation of wax particles);
- Risk assessments / Hazops;
- CFD work on bypass and forces on the pig;
- FMECA;
- Pig assembly checks / pig build quality.

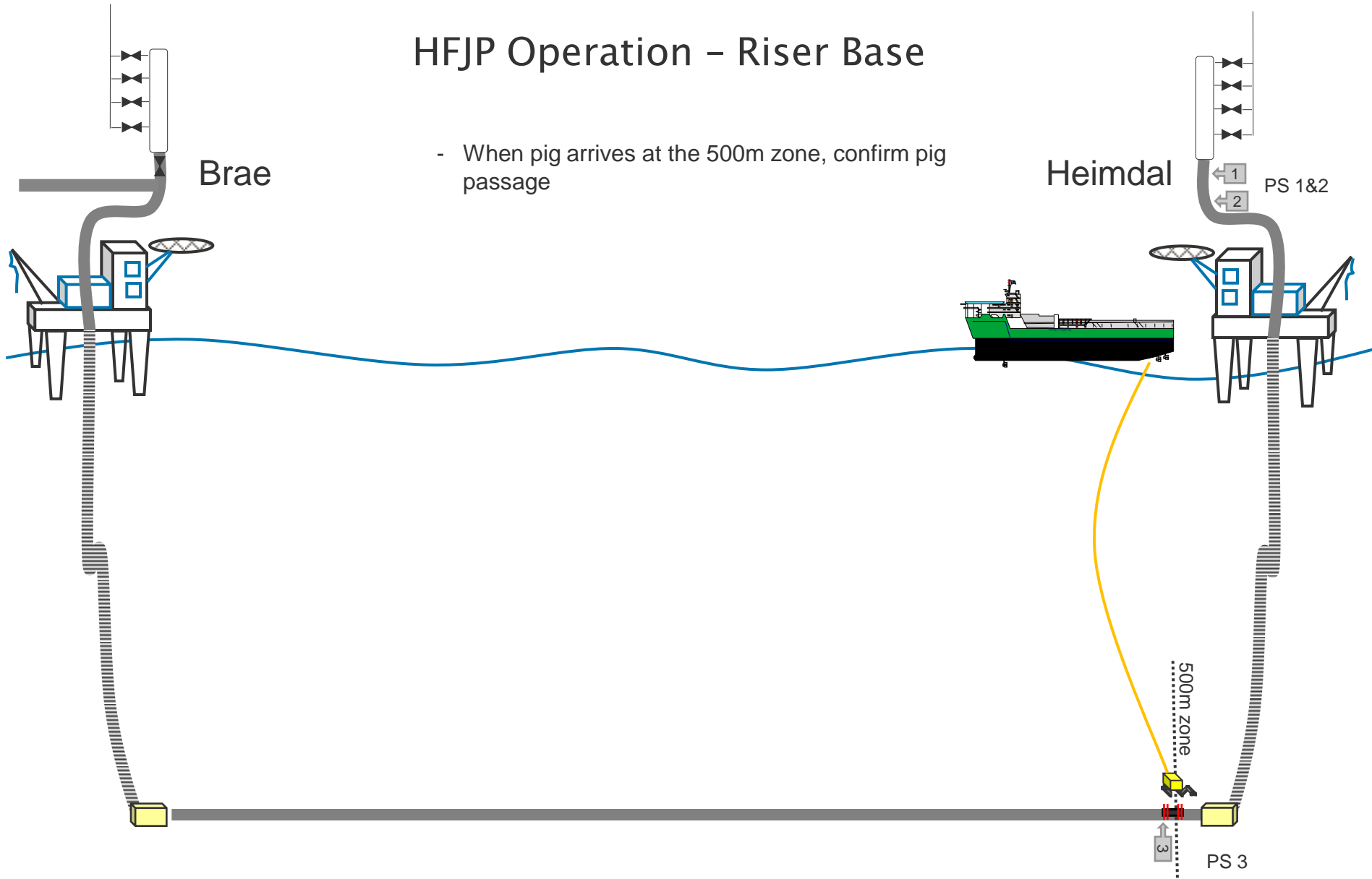


HFJP Operation – Launch January 2013

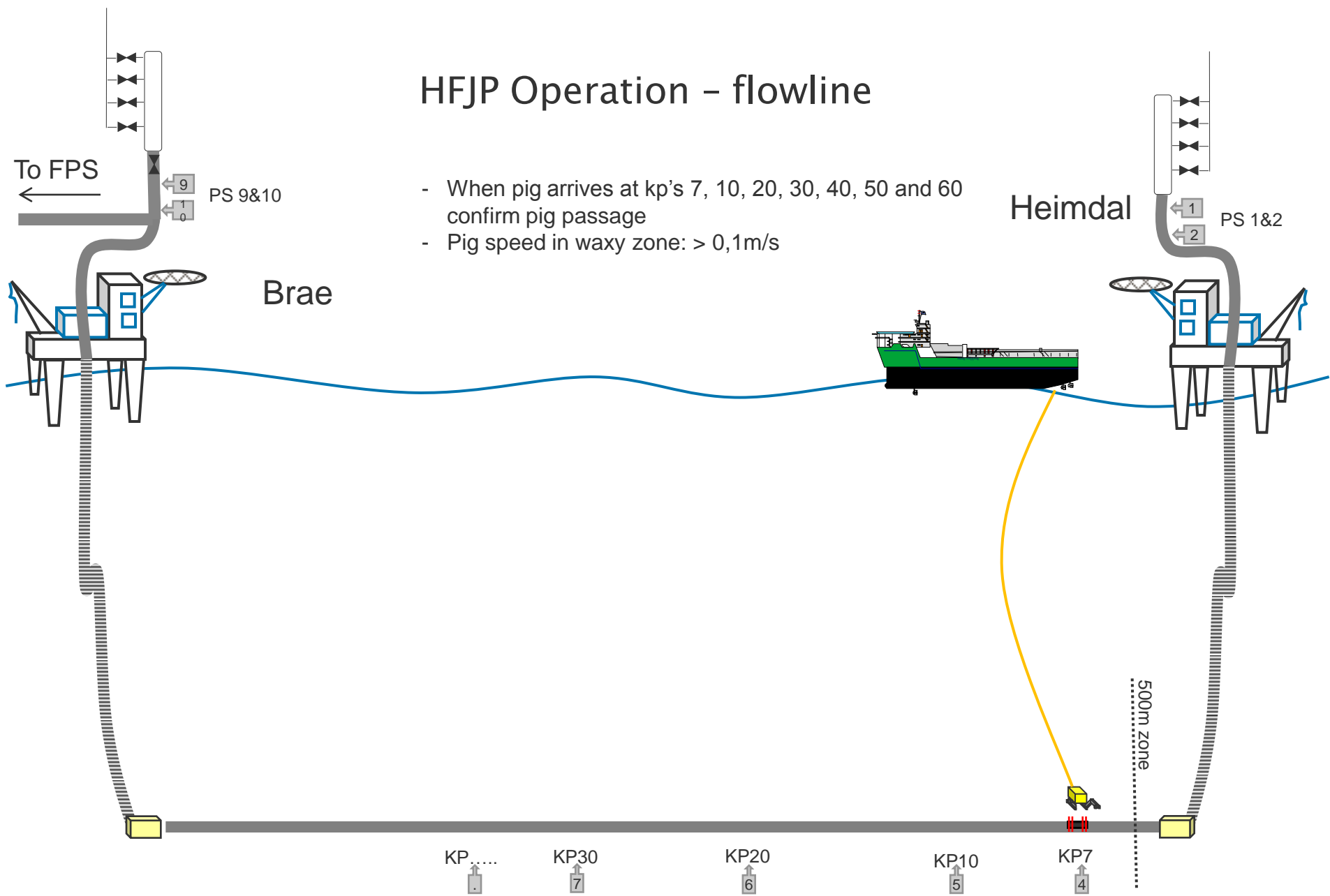


HFJP Operation – Riser Base

- When pig arrives at the 500m zone, confirm pig passage



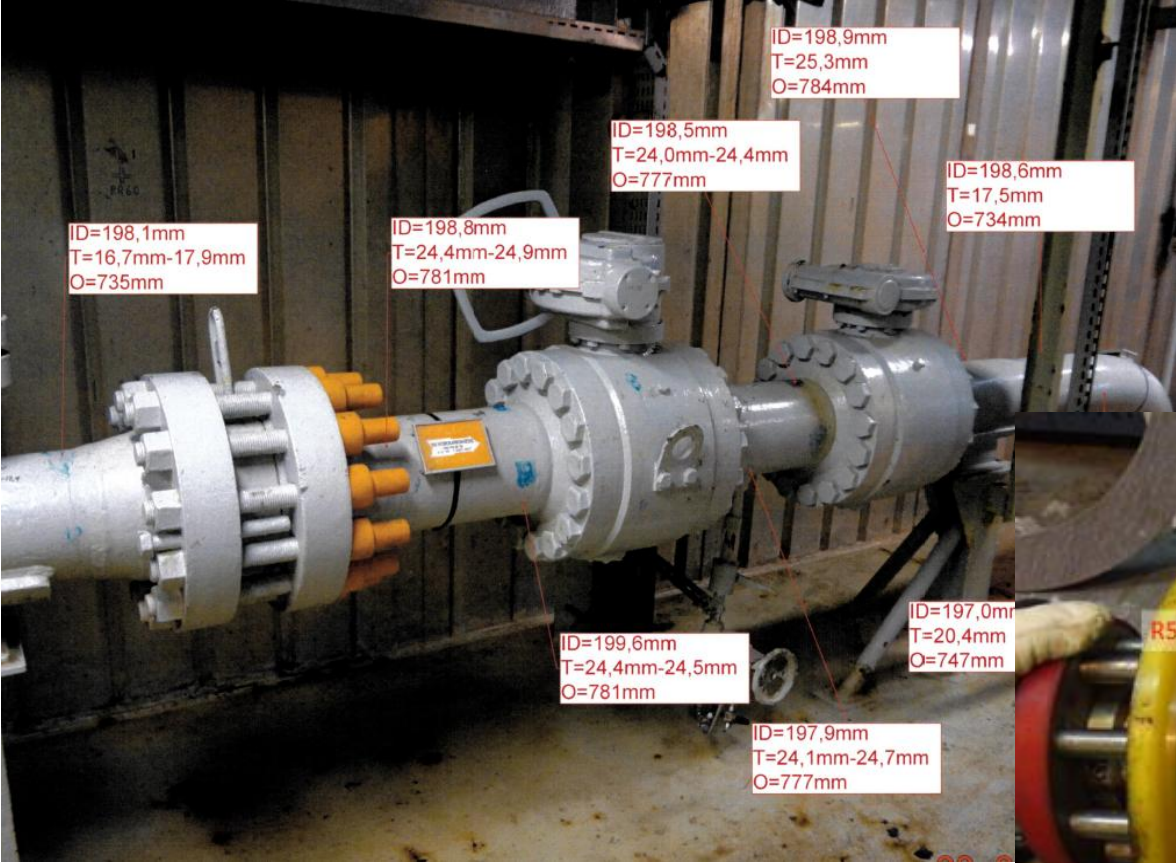
HFJP Operation – flowline



Procedures – monitoring of pressures and flow

	Scenario 1	Scenario 2	Scenario 3	Scenario 4	Scenario 5	Scenario 6	Scenario 7
Flow	Steady	Steady	Increase	Rising / falling	Dropping	Steady	Goes to zero
Line Inlet Pressure	Falling slowly	Steady	Falling slowly	Erratic	Rising	Rises to 180bars max	Rises to 180bars max
Line DP	Falling Slowly	Steady	Falling Slowly	Erratic	Rising	Rises 124bar max	Rises 124bar max
Action	Ideal, no action	Monitor, no action	Monitor, no action	Expected behaviour	Reduce Inlet Pressure, 20bar DP increase maximum	Reduce flow and monitor closely. Plan to continue	Stop flow. Reverse

Initial Pig run

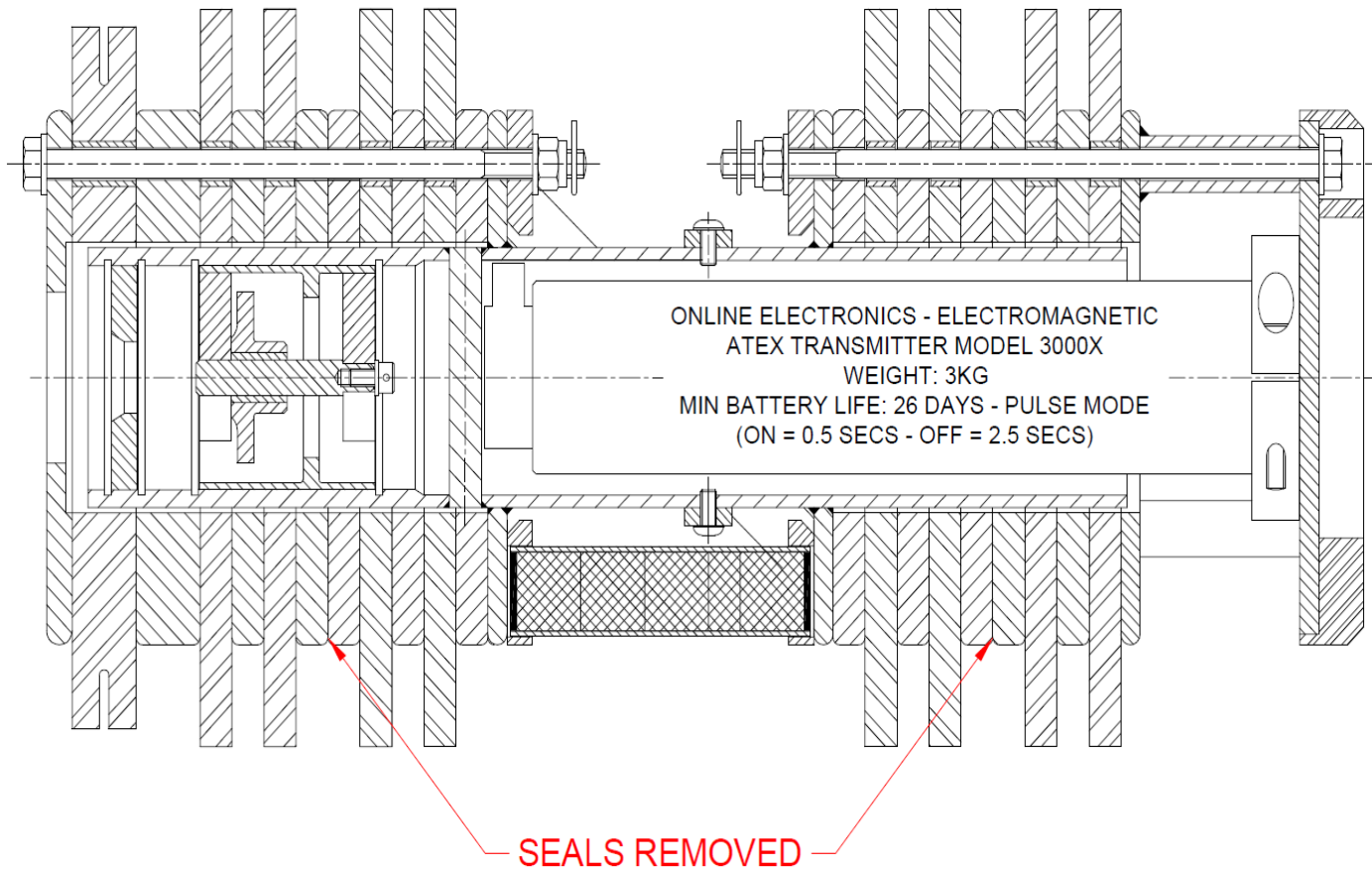


Pig stalled topside due to mislaunch through the eccentric reducer



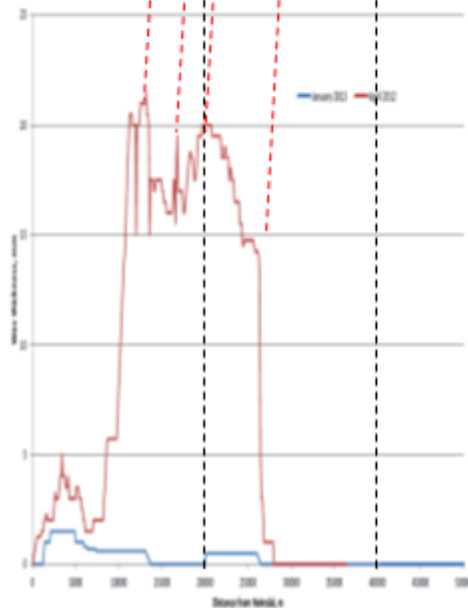
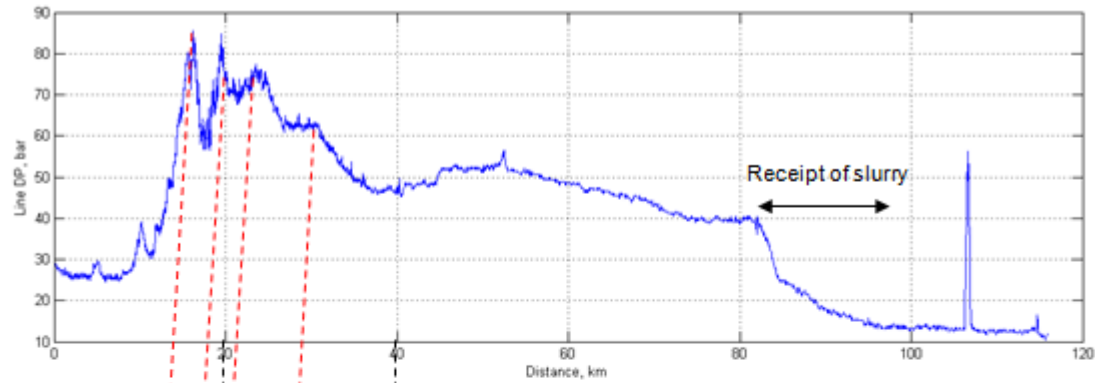
Modified Pig Design

← PIGGING DIRECTION



Line DP during the run

DP

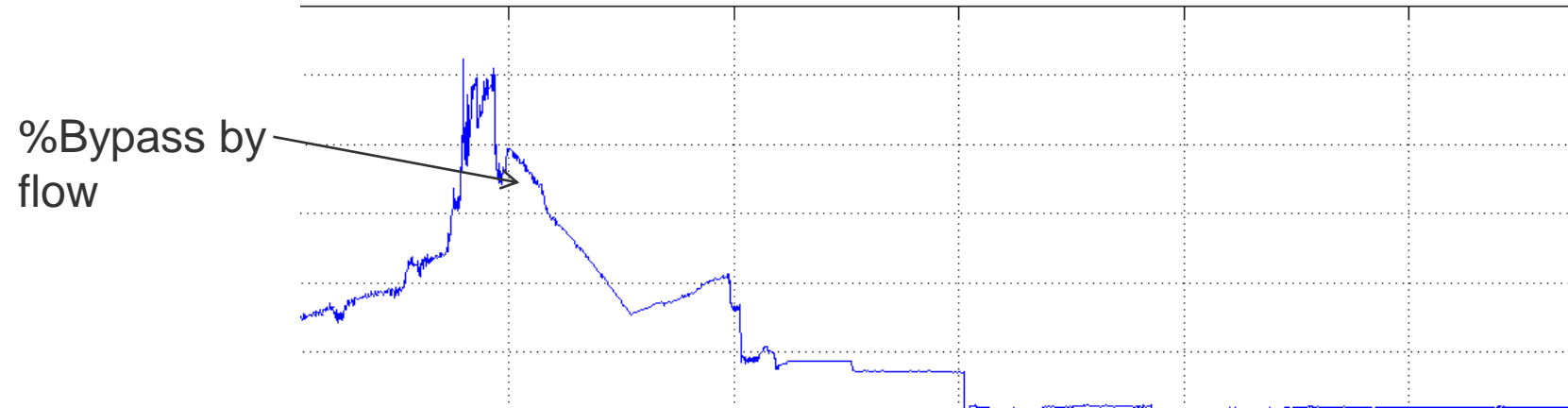
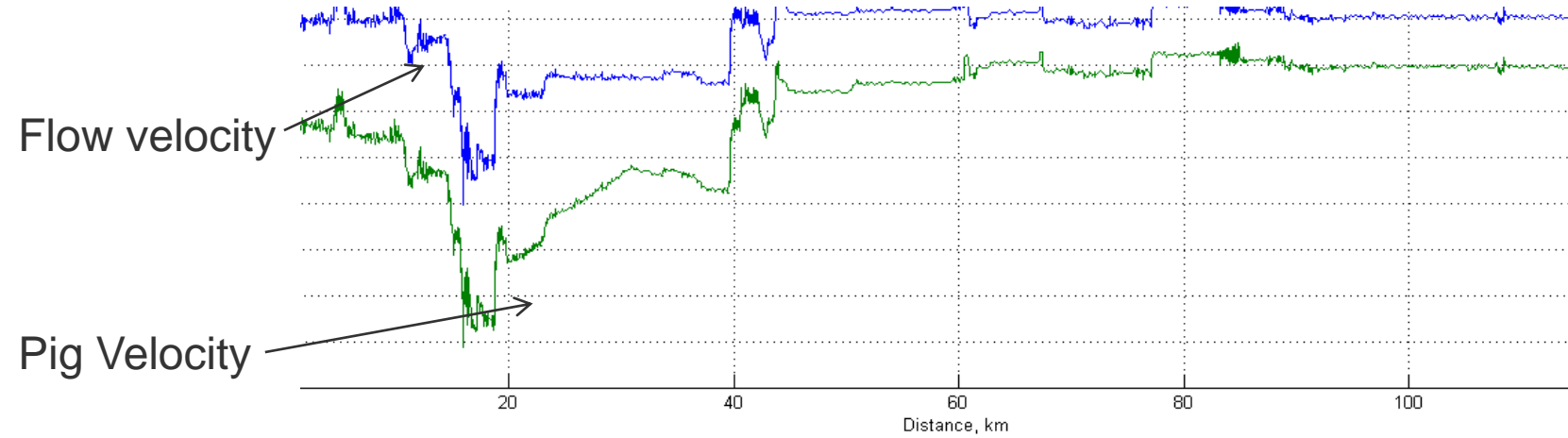


Wax thickness

Pig Location against time



Pig Velocity against distance

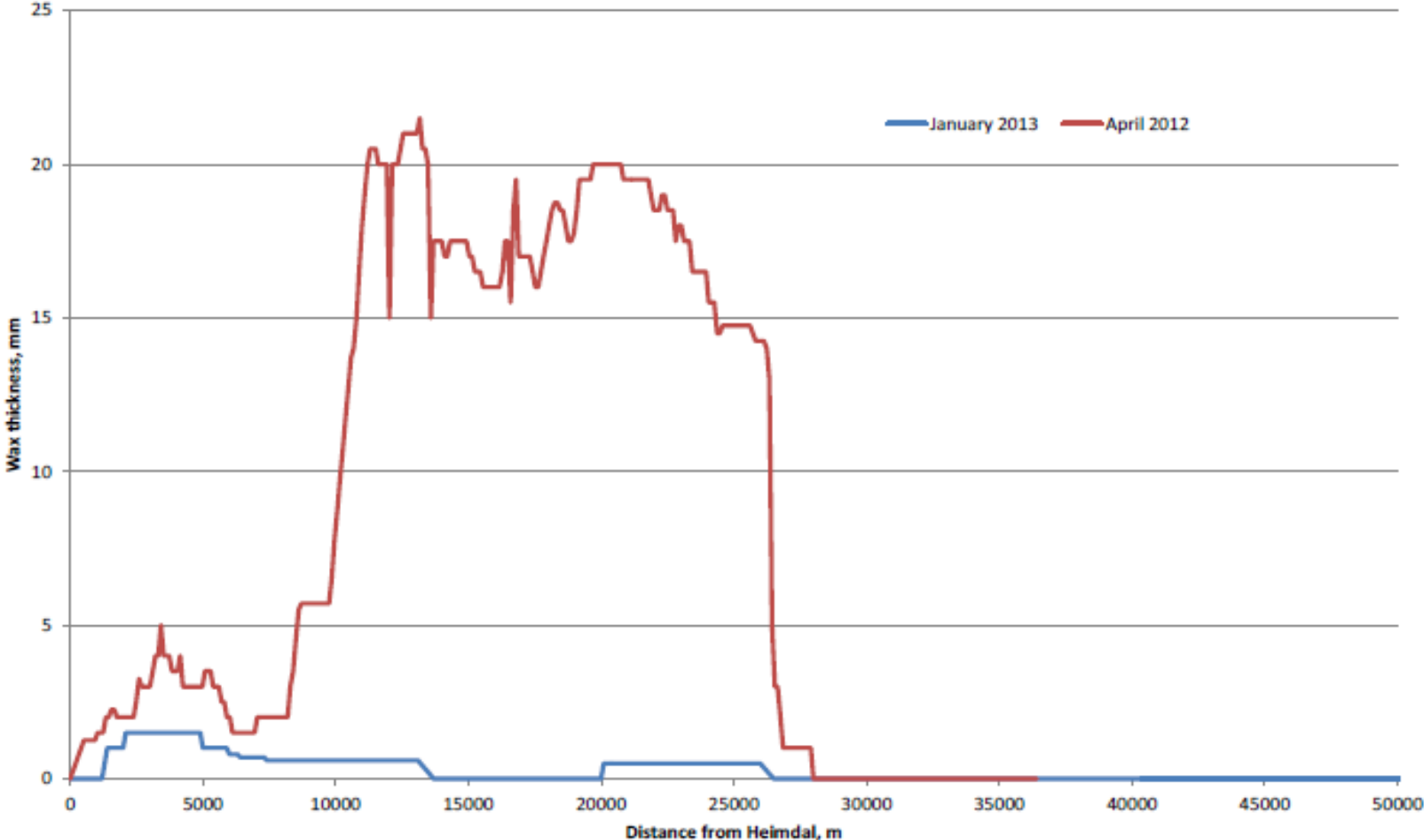


Lessons and observations

- Isotopes would be better for location of pig topside;
- Magnetic signaller worked very well subsea;
- Monitoring of flows and pressures / pig location fed in well to the analysis of the pig run in real time;
- Understanding of the flow rate ranges and controllability of the flows is key to the operation;
- Control of outlet pressures and conditions would be good but not always possible (complex system);
- Shuttle valve for reversal was useful during initial mis-launch.



Final Markland test



After the HFJP

- Winter / Spring 2013: 4 operational pigs for wax control, similar design to HFJP
- June 2013: 1 pre-inspection scraper pig + 1 operational pig



X 4 +



- June 2013: Inspection pig from Rosen Pipeline approved!!



Cake!



There's never been a better
time for **good ideas**

Presentation title

Presenters name

Presenters title

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